

AMENDMENTS TO THE SPECIFICATIONIN THE ABSTRACT OF THE DISCLOSURE

Attached hereto is a replacement Abstract with markings to show amendments.

IN THE WRITTEN DESCRIPTION

Please replace paragraphs [0030]-[0031] with the following amended paragraphs:

[0030] 4 cm<sup>3</sup> of each of these catalysts was packed into a fixed-bed flow reactor with a length in the vertical direction of 50 cm and an inside diameter of 1 cm, soy bean oil (produced by Kanto Chemical) as the raw material ester and methanol as the alcohol were introduced from the upper end, and the conversion rate of soy bean oil at the lower outlet was measured by gas chromatography 4 and 20 hours after the start of the feed. The molar ratio of soy bean oil to methanol was 1:40. The results are shown in Table 1.

Table 1

Experimental example	1	2
Experimental number	28-7	5-7
Catalyst	MO-858	MO-817
Reaction temperature (°C)	200	200
WHSV (1/hour)	1.85	1.85
Raw material flow rate (g/hour)		
Soy bean oil	3.0	3.0
<del>Ethanol</del> Methanol	4.4	4.4
Soy bean oil conversion rate (%)		
After 4 hours	16.0	69.0
After 20 hours	12.0	67.0

[Esterification reaction]

[0031] 4 cm<sup>3</sup> of each of these catalysts was packed into a fixed-bed flow reactor with a length in the vertical direction of 50 cm and an inside diameter of 1 cm, octanoic acid as the raw material fatty acid (produced by Kanto Chemical) and

methanol as the alcohol were introduced from the upper end, and the conversion rate of octanoic acid at the lower outlet was measured by gas chromatography ~~4 and 208~~ hours after the start of the feed. The molar ratio of octanoic acid to methanol was 1:4.5. The results are shown in Table 2.

Table 2

Experimental example	3	4	5	6
Catalyst	MO-858	MO-817	MO-858	MO-817
Reaction temperature (C°)	105	105	90	90
WHSV (1/hour)	1.5	1.5	1.5	1.5
Raw material flow rate (g/hour)				
Octanoic acid	3.0	3.0	3.0	3.0
Methanol	3.0	3.0	3.0	3.0
Octanoic acid conversion rate (%) after 8 hours	97.7	99.3	93.4	94.6